

Molecular Interaction for the binary system of o-chloro phenol with methanol, ethanol, 1-propanol and 2-propanol at 298.15K by measuring the densities and viscosities

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Abstract

this project are studied the molecular interaction for the binary system that is contained o-chlorophenol with methanol, ethanol, 1-propanol, and 2-propanol by measuring the densities, and viscosities than conferred this to excess molar quantities by get the excess molar volume and deviation from viscosities and explain this by two figure. Then get the standard deviation and parameters to the equation of polynomial by using Redlick –Kister form.

Interdiction

There is many studies that is taken methanol, ethanol, 1-propanol, 2-propanol, with polar and non polar solvents like water, alcohols, ethers, but there is less than studied. With the cyclic substitution compound so we get the cyclic aromatic compound that is contained two conditions the first are it contained hydroxyl group that is forming phenol. and the second are chloride ion in para region and that is get stability for the o-chlorophenol one of the ⁽¹⁾ studied molecular interaction for the binary system of 2-propoxyethanol and 2-isopropoxyethanol with methanol, 1-propanol, 2-propanol and 1-pentanol at 298.15K by excess molar volumes and viscosities and that is show negative deviation for this system except 1-pentanol

in another project that ⁽²⁾ studied the molecular interaction for the project of γ -butyrolactone with methanol, ethanol, 1-butanol, and 1-octanol in 298.15K by measured the relative permittivity (ϵ), densities (ρ), refractive indices (n_D) and ultrasonic velocities (u), that is show molecular interaction was very clear and literature. ⁽³⁾ were measured Densities and viscosities

For the binary mixtures (methanol, ethanol, 1-propanol, and 2-propanol with Nitromethane) at temperatures from 293.15K to 313.15K by the excess molar quantities that is show two kind of deviation from ideality

At last project were ⁽⁴⁾ studied the same alcohols with synthetic C_6 + Mixture from 298.15K to 318.15K by densities and viscosities properties and they got the same result

Materials

In table (1) the compound that is used in project and the purity and the source of the compound

| Compound | Company | Purity |
|----------------|----------|--------|
| o-chlorophenol | RDSH* | 99% |
| Methanol | Merck | 99.8% |
| Ethanol | Merck | 99.8% |
| 1-propanol | S.R.L.** | 99.5% |
| 2-propanol | S.R.L. | 99.8% |

*H.M. Rosentock, K.Draxl, B.W. Steiner, and J.T. Herron

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O-chlorophenol was fractionally distilled over Zn powder the middle fraction redistilled over BaO and the middle colorless fraction collected all the alcohol were partially degassed at low pressure and dried over 0.4 nm molecular sieves (Fluka, AG) the results of the measurements of their densities and viscosities at (298.15)K and atmospheric pressure are given in table (2) with some values taken from the literature which agreed with it

Table (2) experimental value of densities and viscosities for the component in this studies and in the reference at (298.15) K.

| Compound | Exp. density | Ref. density | Exp. viscosity | Ref. viscosity |
|----------------|--------------|------------------------|----------------|------------------------|
| o-chlorophenol | 1.25861 | 1.25854 ⁽⁵⁾ | 3.38117 | 3.3813 ⁽⁵⁾ |
| Methanol | 0.78639 | 0.78637 ⁽⁶⁾ | 0.55134 | 0.5513 ⁽⁶⁾ |
| Ethanol | 0.78670 | 0.78628 ⁽⁷⁾ | 1.08965 | 1.087 ⁽⁴⁾ |
| 1-propanol | 0.79931 | 0.79958 ⁽⁸⁾ | 1.93148 | 1.927 ⁽¹⁰⁾ |
| 2-propanol | 0.78032 | 0.78090 ⁽⁹⁾ | 2.04434 | 2.0436 ⁽¹⁰⁾ |

The uncertainty in the mole fraction is $\pm 5 \times 10^{-5}$. all the solutions of different composition were prepared by mass in a 25cm³ Erlenmeyer Flask provided with a joint stopper using a Mettler AB204 balance with an uncertainty of ± 0.1 mg

For the densities used water bath model (mgw LAUDAM3) for KRUSS company with thermometer to get a high accuracy in ($\pm 0.01^\circ$), and using pycnometer constant volume (5cm³) with stopper contained capillary tube

To measure the viscosities used viscometer from (Schott-Gerate) model (AVS-300) with computerized system to calculate the (flow time) (t). that is joined with two photo cells by climb and this climb were fixed inside the bath water from (Schott-Gerate CT 1150) with thermostat and thermometer to get (298.15K) the precision in the temperature was ($\pm 0.01^\circ$)

Results

The excess molar volumes⁽¹¹⁾ (V_m^E) for o-chlorophenol+methanol, ethanol, 1-propanol and 2-propanol, at 298.15K were get by used the following equation

$$V_m^E = \frac{X_1 M_1 + X_2 M_2}{\rho_m} - \frac{X_1 M_1}{\rho_1} - \frac{X_2 M_2}{\rho_2} \quad (1)$$

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Where X_1, X_2 are the mole fractions for o-chlorophenol (X_1), and another alcohols (X_2), M_1, M_2 , are the molar masses for o-chlorophenol and alcohols respectively, ρ_m, ρ_1, ρ_2 is the densities for mixture, and for the pure o-chlorophenol and alcohols

The result of measurements of V^E excess molar volumes are listed in table (3) and graphically represented in figure (1)

From viscosities found the deviation of the viscosities ($\Delta\eta$)⁽¹²⁾ by using the following equation

$$\Delta\eta = \eta_m - \eta_1 X_1 - \eta_2 X_2$$

(2) Where η_m, η_1, η_2 are the dynamic viscosity of the mixture, o-chlorophenol, and alcohol for the pure component respectively the results of ($\Delta\eta$) deviation of the viscosities are listed in table (3) and graphically represented in figure (2)

Table (3):-density, viscosity, excess molar volume, and deviation of viscosity for the binary system of o-chlorophenol (X_1)+methanol, ethanol, 1-propanol, and 2-propanol (X_2) at 298.15 K

Methanol (X_2)

| X_1 | $\rho / \text{g.cm}^3$ | $\text{cp}\eta /$ | V^E | $\Delta\eta$ |
|--------|------------------------|-------------------|--------|--------------|
| 0.1034 | 0.87805 | 0.93844 | -0.106 | 0.094 |
| 0.2132 | 0.95762 | 1.32266 | -0.188 | 0.168 |
| 0.3269 | 1.02517 | 1.70341 | -0.229 | 0.227 |
| 0.4008 | 1.06252 | 1.92653 | -0.225 | 0.241 |
| 0.5398 | 1.12293 | 2.33188 | -0.223 | 0.253 |
| 0.6187 | 1.15213 | 2.53815 | -0.201 | 0.236 |
| 0.7041 | 1.18053 | 2.74182 | -0.172 | 0.198 |
| 0.7634 | 1.19797 | 2.90063 | -0.115 | 0.188 |
| 0.8129 | 1.21217 | 3.01071 | -0.101 | 0.159 |
| 0.8740 | 1.22872 | 3.13761 | -0.089 | 0.113 |
| 0.9461 | 1.24673 | 3.29664 | -0.065 | 0.068 |

Ethanol (X_2)

| X_1 | $\rho / \text{g.cm}^3$ | η / cp | V^E | $\Delta\eta$ |
|-------|------------------------|--------------------|---------|--------------|
| 0.095 | 0.85014 | 1.36021 | -0.0763 | 0.051 |
| 0.210 | 0.92013 | 1.69293 | -0.147 | 0.12 |
| 0.320 | 0.98055 | 1.99177 | -0.1742 | 0.167 |
| 0.401 | 1.02110 | 2.21163 | -0.179 | 0.204 |
| 0.518 | 1.07633 | 2.50581 | -0.161 | 0.228 |
| 0.612 | 1.11662 | 2.71351 | -0.125 | 0.221 |

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| | | | | | |
|---|-------|---------|---------|---------|-------|
| 9 | 0.681 | 1.14478 | 2.87313 | -0.091 | 0.22 |
| 5 | 0.748 | 1.17032 | 3.01285 | -0.0504 | 0.208 |
| 6 | 0.805 | 1.19155 | 3.12069 | -0.032 | 0.185 |
| 1 | 0.856 | 1.20976 | 3.19992 | -0.0218 | 0.148 |
| 1 | 0.931 | 1.23566 | 3.31048 | -0.003 | 0.087 |

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1-propanol (X₂)

| X ₁ | ρ/g.cm ³ | η/cp | V ^ε | Δη |
|----------------|---------------------|---------|----------------|---------|
| 0.1066 | 0.83758 | 2.16301 | -0.059 | 0.077 |
| 0.1911 | 0.88052 | 2.33351 | -0.108 | 0.125 |
| 0.2802 | 0.92485 | 2.48268 | -0.125 | 0.145 |
| 0.3286 | 0.94860 | 2.56384 | -0.127 | 0.156 |
| 0.4689 | 1.01608 | 2.76024 | -0.103 | 0.149 |
| 0.5631 | 1.06050 | 2.87081 | -0.081 | 0.123 |
| 0.6391 | 1.09553 | 2.94597 | -0.039 | 0.088 |
| 0.7173 | 1.13148 | 3.02534 | -0.021 | 0.054 |
| 0.8253 | 1.18013 | 3.12610 | 0.024 | -0.0018 |
| 0.9107 | 1.21857 | 3.23881 | 0.0239 | -0.0129 |
| 0.9514 | 1.23679 | 3.29721 | 0.019 | -0.0135 |

2-propanol (X₂)

| X ₁ | ρ/g.cm ³ | η/cp | V ^ε | Δη |
|----------------|---------------------|---------|----------------|---------|
| 0.0894 | 0.82805 | 2.23259 | -0.048 | 0.0687 |
| 0.1606 | 0.86488 | 2.35743 | -0.0763 | 0.0984 |
| 0.2346 | 0.90246 | 2.47196 | -0.0878 | 0.114 |
| 0.3198 | 0.94495 | 2.59885 | -0.0918 | 0.127 |
| 0.4092 | 0.98853 | 2.70437 | -0.0756 | 0.113 |
| 0.4918 | 1.02806 | 2.78259 | -0.0564 | 0.0808 |
| 0.5734 | 1.06638 | 2.85987 | -0.031 | 0.049 |
| 0.6598 | 1.10622 | 2.92468 | 0.0027 | -0.0017 |
| 0.7393 | 1.14231 | 2.98263 | 0.031 | -0.05 |
| 0.8175 | 1.17743 | 3.06069 | 0.046 | -0.0764 |
| 0.9231 | 1.22445 | 3.20596 | 0.038 | -0.0724 |

V^ε

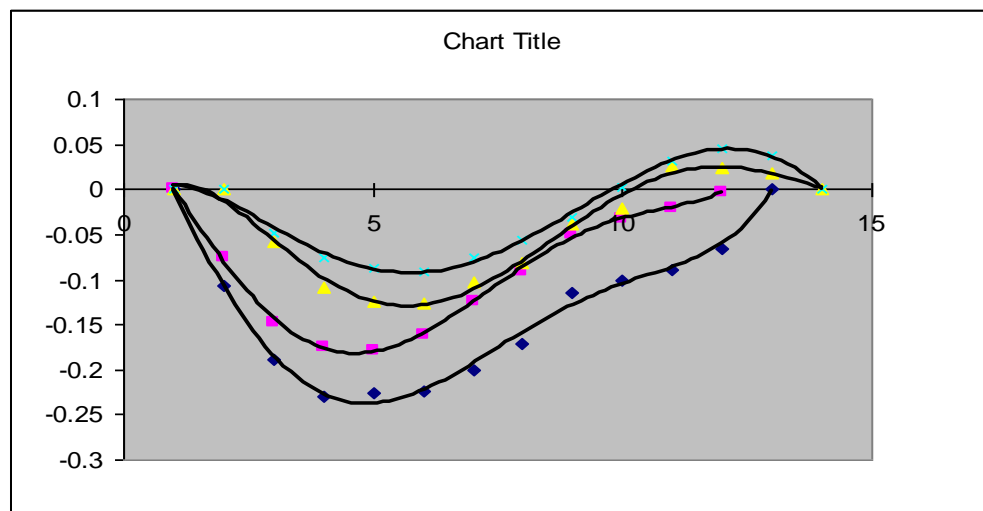


Figure (1) Excess molar Valium V^ε with mole fraction for o-chlorophenol (X₁) with (♦)methanol, (■)ethanol, (▲)1-propanol, (×)2-propanol at 298.15K .

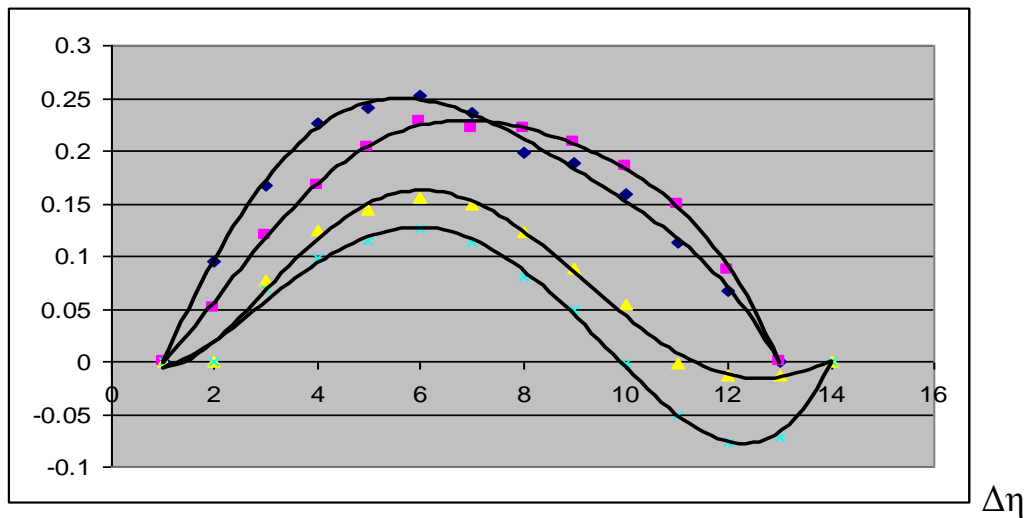


Figure (2) Diviation in viscosity for o-chlorophenol (X_1) with (♦) methanol, (■)ethanol, (▲)1-propanol, (×) 2-propanol at 298.15K

The excess molar volumes and deviations in viscosity were represented mathematically by the Redlich –Kister equation ⁽¹³⁾

$$Y_{(x)} = X_1 (1 - X_1) \sum A_i (X_1 - X_2)^i \quad (3)$$

Where Y^E is V^E , or $\Delta\eta$, X_1 is the mole fraction of alcohol, and (A_i) are the coefficients of the polynomial equation .the values of coefficients (A_i) were determined by a multiple regression analysis based on the least –squares method and were summarized along with the standard deviations between the experimental and fitted values of the respective functions in table(4) the corresponding standard

Deviation was defined by equation.

$$\delta = [(Y_{ex} - Y_{cal})^2 / m - n]^{1/2} \quad (4)$$

Where m is the number of experimental points

Table (5): standard deviation and parameter of equation of polynomial

| Methanol | | | | | |
|--------------|--------|--------|-------|--------|----------|
| system | A_0 | A_1 | A_2 | A_3 | δ |
| V^E | -0.88 | 0.35 | -0.15 | -0.015 | 0.014 |
| $\Delta\eta$ | 0.9 | 0.5 | 0.25 | 0.0564 | 0.0093 |
| Ethanol | | | | | |
| V^E | -0.64 | 0.55 | 0.29 | -0.1 | 0.005 |
| $\Delta\eta$ | 0.88 | 0.4 | 0.2 | 0.056 | 0.007 |
| 1-propanol | | | | | |
| V^E | -0.384 | 0.6 | 0.27 | -0.03 | 0.0065 |
| $\Delta\eta$ | 0.56 | -0.538 | -0.38 | -0.05 | 0.0041 |
| 2-propanol | | | | | |
| V^E | -0.212 | 0.61 | 0.247 | 0.05 | 0.003 |
| $\Delta\eta$ | 0.32 | -0.75 | -0.46 | -0.55 | 0.0066 |

Discussion

The choice of o-chlorophenol has been based on its limited polymerization through

Intermolecular hydrogen bonding in the pure state for molecules of (o-chlorophenol) the addition of alcohols causes another effect of interaction ((intramolecular))

The rupture of intramolecular and intermolecular hydrogen bonding in o-chlorophenol and this will be followed by association of unlike molecules through inter-molecular hydrogen bonding

TO the deviation from ideal mixing are attributed to the desorption forces (14-15) In most theories of the behavior of non-electrolyte solutions the major contribution

In such theories the deviations are expected to be positive .

Negative deviation from ideal behavior in mixtures of molecules of different size can be accounted for by geometric considerations.

Attempts have been made to explain the behavior of liquid mixtures on the basis of sign and magnitude of the excess volumes V^E .

A negative value of V^E indicates strong interaction between the components of the mixtures while positive values are indicative of weaker interaction then strength of interaction between the unlike molecules increases, so V^E becomes increasingly negative .

Figures (1) show negative V^E with well marked maxima at (0.3) and (0.4) mole fractions of o-chlorophenol respectively . the negative values of V^E for the liquid systems are well explained in terms of the dipole-dipole interaction between them.

According to Fort and Moore⁽¹⁶⁾ the values of $\Delta\eta$ are positive for the systems in which desorption forces are dominant, becoming less positive and then increasingly negative in (1-propanol), (2-propanol) as the strength of interaction decreases .

Figure (2) shows that the value of $\Delta\eta$ are positive at the first in all the systems and it is only positive in (methanol), and (ethanol)

So the resolution⁽¹⁷⁾ of the excess molar volume and deviation from viscosities can be explained as (i) specific interaction between the unlike molecules, and (ii) geometric effect

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**التداخلات الجزيئية للنظام ثنائي المكون من أورثو-كلوروفينول مع الميثانول
والإيثانول ١-بروبانول و٢-بروبانول عند درجة حرارة ٢٩٨,١٥ وذلك بقياس الكثافة
واللزوجة**

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الخلاصة

في هذه الدراسة درست التداخلات الجزيئية للنظام الثنائي المكون من الأورثو-كلوروفينول مع كحولات الميثانول، الإيثانول، ١-بروبانول، و٢-بروبانول حيث قيست الكثافة واللزوجة ولمدى كامل من الكسور المولية والتي حولت إلى الكميات المولية الفائضة فوجد الحجم المولي الفائض وانحراف اللزوجة عن المثالية والتي وضحت باستخدام الرسوم البيانية كما استخدمت معادلة Redlik - Kister لحساب الانحراف المعياري ومعاملات المعادلة متعددة الحدود